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**AFFINITY PURIFICATION AND CHARACTERIZATION OF  
CHELATING PEPTIDES FROM CHICKPEA PROTEIN HYDROLYSATES**

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27 **ABSTRACT**

28 A chickpea protein hydrolysate produced with pepsin and pancreatin was  
29 used for the affinity purification of chickpea chelating peptides. Three chelating  
30 peptide fractions were obtained after affinity chromatography with immobilized  
31 copper. These peptide fractions showed a higher chelating activity and histidine  
32 contents than the original protein hydrolysate. Chelating activity was positively  
33 correlated with the histidine content of the purified fractions. Different  
34 subfractions were also obtained after gel filtration chromatography from the  
35 affinity purified peptide fractions. Some of these subfractions showed a higher  
36 chelating activity and histidine contents than the original fractions. These results  
37 suggest that a combination of high His contents, around 20–30%, and small  
38 peptide size provide the best chelating activities. Thus sequential purification  
39 with affinity and gel filtration chromatography is a useful procedure for the  
40 purification of chickpea peptides with high chelating activity. These results show  
41 that a range of chelating peptides are generated during digestion of the  
42 chickpea proteins that, after metal chelation, may prevent the generation of  
43 reactive oxygen species (ROI) and favour metal absorption.

44 **KEYWORDS:** Chelating peptides; Chickpea; Protein Hydrolysate;  
45 Pepsin; Pancreatin.

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51        **1. INTRODUCTION**

52            Chickpea (*Cicer arietinum* L.), is an important source of proteins in  
53 human nutrition in developing countries. Its protein content range from 15 to  
54 25% with a high nutritional quality. Chickpea is extensively grown in different  
55 parts of the world such as India, Mexico and the Mediterranean Region. About  
56 20% of chickpea seeds are damaged during the harvest and processing, and  
57 considered as a by-product that is sold at low prices for livestock feeding (Ulloa,  
58 Valencia, & Garcia, 1988). However, these seeds may be an interesting source  
59 of proteins for the production of protein hydrolysates (Clemente, Vioque, Sánchez-  
60 Vioque, Pedroche, Bautista, & Millán, 1999) and bioactive peptides (Megías *et al.*,  
61 2004).

62            Bioactive peptides are small protein fragments, with beneficial biological  
63 activity, after they are released during gastrointestinal digestion or by previous  
64 *in vitro* protein hydrolysis (Gobbetti, Stepaniak, De Angelis, Corsetti, & Di  
65 Cagno, 2002; Pihlanto & Korhonen, 2003; Vioque *et al.*, 2000). Bioactive  
66 peptides have been studied mainly in milk and derived products such as cheese  
67 or yogurt. In addition, their existence has been observed in other animal and  
68 also plant proteins such as soy, rice, chickpeas and even in fungi. Bioactive  
69 peptides with different functions such as antihypertensive, immunomodulatory,  
70 opioid, antioxidant, hypocholesterolemic, or metal chelating activity have been  
71 described (Vioque *et al.*, 2000; Gobbetti *et al.*, 2002).

72            Metals are capable of producing reactive oxygen species (ROS) causing  
73 damage to biomolecules, diseases such as cardiovascular disease, atherosclerosis,  
74 cancer, neurological degenerative diseases, and others (Gaetke and Chow,  
75 2003). In addition, ROS have a negative impact in flavor, texture, nutritive value,

76 and shelf life of food products and, under extreme conditions, produce toxins.  
77 Chelating peptides may prevent this pro-oxidant effect by metal ion chelation.  
78 Also, bioavailability of minerals represent a nutritional problem for different  
79 sectors of the population such as children, elderly, and women in the first world.  
80 Food fortification with the addition of minerals in the form of salts has been  
81 proposed to reduce these deficiencies (Zhu et al., 2006). However, this have  
82 some limitations such as ions low solubility, oxidative reactions and modification  
83 of the flavour and colour of the fortified food. Thus the addition of minerals in the  
84 form of chelates may improve minerals bioavailability. Chelating peptides may  
85 be an alternative to increase mineral bioavailability. Thus, the positive effect of  
86 chelating phosphopeptides, derived from milk proteins, on the absorption of  
87 minerals such as calcium (Cross, Huq, & Reynolds, 2007), zinc (Miquel & Farre,  
88 2007) and iron (Bouhallab et al., 2002) have been reported. Hence, chelating  
89 peptides, purified from vegetables protein hydrolysates, may also facilitate the  
90 bioavailability of these minerals.

91 Bioactive peptides are usually purified from protein hydrolysates by  
92 several chromatographic steps including FPLC gel filtration and C<sub>18</sub> RP-HPLC  
93 chromatography. Affinity chromatography is a powerful protein purification  
94 technique that relies on the formation of specific reversible complexes between  
95 the molecule to be purified and an immobilized ligand. After incubation of the  
96 affinity adsorbent with the mixture containing the molecule of interest and  
97 washing to remove unbound molecules, the molecules that are retained are  
98 recovered by using specific or nonspecific elution agents.

99 In previous works we have shown that sunflower and chickpea proteins  
100 hydrolyzed with the microbial proteases alcalase and flavourzyme contained

101 peptides with chelating activity, indirectly measured as the ability to inhibit  
102 oxidation of  $\beta$ -carotene in the presence of copper (Megias et al., 2007a Megias  
103 et al., 2007b). In this work a chickpea protein hydrolysate produced with pepsin  
104 plus pancreatin has been used for the purification of chelating peptides by metal  
105 chelating affinity chromatography. Chickpea chelating peptides were further  
106 fractionated by size exclusion chromatography and characterized.

107

## 108 **2. MATERIAL AND METHODS**

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### 110 **2.1. Material**

111 Chickpea seeds (*Cicer arietinum* L.) were purchased in a local market.  
112 Diethyl ethoxymethylenemalonate was purchased from Fluka (Buchs,  
113 Switzerland). Amino acids standards, D,L- $\alpha$ -aminobutyric acid,  
114 trinitrobenzenesulphonic acid (TNBS), ethylenediamine tetra-acetic acid (EDTA),  
115 pepsin, pancreatin and pyrocatechol violet (PV) were provided by Sigma-Aldrich  
116 (St. Louis, MO, USA).

117

### 118 **2.2. Analytical methods**

119 Nitrogen was analyzed in the defatted chickpea flour by Kjeldahl method  
120 in a Foss Kjeltac™ 2300 Analyzer equipped with a Digestion Tecator™ system  
121 (Höganäs, Sweden). Nitrogen was determined in protein isolates using a LECO  
122 CHNS-932 analyzer (Leco Corporation, St. Joseph, MI, USA). Protein content  
123 was calculated using 6.25 as conversion factor. Moisture and ash were  
124 determined using AOAC (1990) 942.05 and 945.39 approved methods,

125 respectively. Soluble sugars were determined according to Dubois et al.,  
126 (1956). Total fiber content was determined according to Lee et al. (1992).

127

### 128 **2.3. Preparation of chickpea defatted flour**

129 Chickpea seeds were ground and defatted with hexane in a soxhlet  
130 extractor for 9 h. The resulting defatted chickpea flour was used as starting  
131 material for production of protein isolates. For this, chickpea flour (20 g) was  
132 suspended in 200 ml sodium sulphite (0.25%) pH 10, and extracted by stirring  
133 for 1 h. After centrifugation two additional extractions were carried out.  
134 Afterwards, the pH of the pooled supernatant was adjusted to the isoelectric  
135 point (pH 4.3) and the precipitate formed was recovered by centrifugation. This  
136 precipitate was washed with distilled water adjusted to pH 4.3 and freeze-dried  
137 until further use.

138

### 139 **2.4. Preparation of chickpea protein hydrolysates**

140 Chickpea protein isolates produced as previously described (Sánchez-  
141 Vioque et al., 1999) were used as substrate for the production of chickpea  
142 protein hydrolysate. Chickpea protein isolates were hydrolyzed sequentially with  
143 pepsin and pancreatin using a hydrolysis reactor vessel (B. Braun Biotech. Int.,  
144 GMBH, Melsungen, Germany) equipped with stirrer, thermometer and pH  
145 electrode. Hydrolysis parameters were as follows: protein isolates  
146 concentration, 5% (w/v); enzyme/substrate ratio 1/20 (w/w); pH 2.5 (pepsin  
147 hydrolysis) or 7.5 (pancreatin hydrolysis); temperature, 37 °C. Pepsin was  
148 added at time 0, and after 180 min, pancreatin was added for another 180 min.  
149 The hydrolysis was inactivated by heating at 80 °C for 20 min. Hydrolysates

150 were clarified by centrifugation, lyophilized and storage at -20 °C until further  
151 use.

152

### 153 **2.5. Degree of hydrolysis**

154 The degree of hydrolysis was calculated by determination of free amino  
155 groups by reaction with TNBS (Adler-Nissen, 1979). The total number of amino  
156 groups was determined in a sample of protein isolate hydrolyzed by treatment  
157 with 6 N HCl at 120 °C for 24 h.

158

### 159 **2.6. Affinity chromatography purification of chelating peptides**

160 100 mg of chickpea protein hydrolysate were dissolved in 10 mL loading  
161 buffer (50 mM pH 7.4 sodium acetate buffer, 0.5 M sodium chloride) and filtered  
162 through 0.22 µm. 10 mL of this hydrolysate solution were loaded on a HiPrep  
163 IMAC FF 16/10 (20 mL) column (GE) that was previously charged with copper  
164 according to manufacturer instructions and coupled to a FPLC AKTA-purifier  
165 system (GE). After loading the sample the column was washed with loading  
166 buffer until absorbance at 280 nm was stabilized. Then, chelating peptides  
167 retained to the column were eluted with a pH gradient from 7.4 to 4.0 in 50 mM  
168 sodium acetate, 0.5 M sodium chloride buffer at 1 mL/min flow. Eluted chelating  
169 peptides were collected and concentrated using a nanofiltration system  
170 (Amicon®, Millipore Corporation, Bedford, EEUU) with a nanofiltration  
171 membrane TFC-SR model 3 (Koch membranes).

172

### 173 **2.7. Gel filtration chromatography of chelating peptides**

174 Purified chelating peptide fractions were further fractioned by gel filtration  
175 chromatography using a Superdex-peptide column coupled to a FPLC AKTA-  
176 purifier system (GE). The eluent used was 0.75 M ammonium bicarbonate  
177 buffer at a flow rate of 0.5 ml min<sup>-1</sup>. Elution was monitored at 215 nm and the  
178 proximate molecular masses of eluted peptides were determined using the  
179 following molecular weights standards from Pharmacia: blue dextran (2000  
180 kDa), cytochrome C (12.5 kDa), aprotinin (6512 Da), bacitracin (1450 Da),  
181 cytidine (246 Da) and glycine (75 Da).

182

### 183 **2.8. Amino acid analysis of chickpea peptides**

184 The amino acids composition of peptide fractions were deter- mined  
185 after amino acids derivatisation with diethyl ethoxymethyl- enemalonate by  
186 HPLC using D,L-a-aminobutyric acid as an internal standard (Alaiz, Navarro,  
187 Girón, & Vioque, 1992). The HPLC system consisted of a model 600E  
188 multisystem with a 484 UV–Vis detector (Waters Corporation, Milford, MA,  
189 EEUU) equipped with a 300 mm × 3.9 mm i.d. reversed-phase column  
190 (Novapack C18, 4 lm; Waters). A binary gradient was used for elution with a  
191 flow of 0.9 ml/min. The solvents used were (A) sodium acetate (25 mM)  
192 containing sodium azide (0.02% w/v), pH 6.0, and (B) acetonitrile. Elution was  
193 as follows: time, 0.0–3.0 min; linear gradient from A/ B (91/9) to A/B (86/14);  
194 3.0–13.0 min, elution with A/B (86/14); 13.0–30.0 min, linear gradient from A/B  
195 (86:14) to A/B (69/31); and 30.0–35.0 min, elution with A/B (69/31). The column  
196 was maintained at 18 °C.

197 Tryptophan was determined after basic hydrolysis according to Yust et al.  
198 (2004). For this, samples were hydrolysed in 3 ml 4 M sodium hydroxide at 100

199 °C for 4 h. Hydrolysates were neutralized to pH 7 and diluted to 25 ml with 1 M  
200 sodium borate buffer (pH 9). Tryptophan was determined by HPLC-RP at 280  
201 nm.

## 202 **2.9 Copper chelating activity of chickpea peptides**

203 Copper chelating activity was determined by copper chelate titration  
204 using pyrocatechol violet (PV) as the metal chelating indicator (Saiga et al.  
205 2003). 100 µL of 0.1 µg/µL CuSO<sub>4</sub> in 50 mM sodium acetate buffer pH 6.0 was  
206 mixed with 25 µL of PV 4 mM in 50 mM sodium acetate buffer pH 6.0. The  
207 complex of PV and Cu<sup>2+</sup> absorbs blue light at 632 nm, while PV dissociated with  
208 a metal ion in the presence of chelating agents does not show this absorption.  
209 Thus, copper chelating activity is proportional to the decrease in absorbance at  
210 632 nm.

211 Chelating activity was calculated according to the following formula:

$$212 \quad \% \text{ Chel.Act.} = (1 - \text{Abs}_{632\text{nm}}(\text{PV} + \text{Cu}^{++} + \text{sample}) / \text{Abs}_{632\text{nm}}(\text{PV} + \text{Cu}^{++})) \\ 213 \quad \times 100 \\ 214$$

215 where Abs<sub>632nm</sub> (PV + Cu<sup>++</sup> + sample) is the absorbance at 632 nm of the  
216 PV + Cu<sup>++</sup> complex in the presence of peptides samples, and Abs<sub>632nm</sub> (PV +  
217 Cu<sup>++</sup>) is the absorbance at 632 nm of the PV + Cu<sup>++</sup> complex in the absence of  
218 peptides samples.

219

## 220 **3. RESULTS AND DISCUSSION**

### 221 **3.1. Production of chickpea protein hydrolysates**

222 A chickpea protein isolate was used as a substrate for the production of  
223 chickpea protein hydrolysates. Table 1 shows the chemical composition of this  
224 protein isolate compared with the composition of the original defatted chickpea

225 flour. The protein isolate, with a protein content above 95% and minor amounts  
226 of other compounds, represent an optimal substrate for the production of  
227 chickpea protein hydrolysates and further purification of bioactive peptides. The  
228 protein hydrolysate was produced by sequential action of the digestive enzymes  
229 pepsin and pancreatin. Fig. 1 shows the kinetic of chickpea protein isolate  
230 hydrolysis. The rate of hydrolysis with pepsin was very high during the first 10  
231 min, and after that hydrolysis proceeded more slowly. After 180 min of  
232 incubation, pepsin produced a protein hydrolysate with 16.3% degree of  
233 hydrolysis, before pancreatin was added. A final protein hydrolysate, obtained  
234 after sequential digestion of chickpea proteins with pepsin and pancreatin, had  
235 a 27.03% degree of hydrolysis. At the end of the hydrolysis, the degree of  
236 hydrolysis decreased from 31.5% to 27.0%, probably due to the plastein  
237 reaction by which proteases catalyses a peptides condensation process,  
238 resulting in protein materials of higher molecular weights (Wil-lians, Brownsell,  
239 & Andrews, 2001).

### 240 **3.2. Purification of chickpea chelating peptides**

241 The chickpea protein hydrolysate produced after hydrolysis with pepsin  
242 and pancreatin was used as substrate for the purification of chelating peptides  
243 by affinity chromatography with immobilized copper. According to the  
244 manufacturer's instructions (GE Healthcare) proteins or peptides bounded to  
245 the metal charged Hi- Prep IMAC FF 16/10 column can be eluted with a linear  
246 gradient from pH 7 to 4. Therefore, bounded chickpea chelating peptides were  
247 eluted from the copper charged column with a pH gradient from 7.4 to 4 (Fig. 2).  
248 Three chelating peptides fractions (F1, F2 and F3), that eluted with different  
249 acidic pH values, were collected. The use of a cromatography column and a pH

250 gradient in the eluting buffer allowed the purification of different peptide  
251 fractions with increasing affinity for the solid support. This is in contrast to our  
252 previous results using metal chelate spin columns that provided only a single  
253 fraction of chelating peptides after centrifugation of the columns for elution of  
254 the bounded peptides (Megías et al., 2007a, 2007b).

255 Table 2 shows the amino acid composition of the chickpea protein hydrolysate  
256 and the three purified chelating peptide fractions (F1, F2 and F3) from the  
257 copper affinity column. Fractions F1 to F3 showed different amino acid  
258 compositions that explain their different degrees of binding to the affinity col-  
259 umn. For example, F1 was especially rich in Arg and Lys and F3 in Ser. Also a  
260 positive correlation between His contents and elution volume from the affinity  
261 column was observed in these fractions (Fig. 3). Thus fraction F1, with His  
262 contents similar to the observed in the protein hydrolysate, eluted first at the  
263 beginning of the pH decreasing gradient. The high amounts of Arg and Ser may  
264 be the responsible of the interaction of this fraction with the solid support. After  
265 fraction F1, eluted fractions F2 and F3 with lower pH eluting values and  
266 increasing His contents. His, due to its imidazole ring, may be directly  
267 implicated in the peptide binding to the copper containing affinity column.  
268 Swain, Tabatabai, and Reddy (2001) also observed a positive correlation  
269 between the elution volume and His contents of chelating peptide fractions  
270 purified from a beef protein hydrolysate produced with pepsin plus pancreatin.  
271 Chelating peptide fractions F1, F2 and F3 were further fractionated, by gel  
272 filtration chromatography, into subfractions of different molecular weights (Fig.  
273 4). Table 3 shows the proximate molecular weight of these subfractions. Main  
274 subfraction of F1 fraction, F1B, has an average of 40 amino acids. On the

275 contrary in F2 main subfraction, F2B, was 11 amino acid long, and in F3 was  
276 5 aminoacids long (F3C).

277 Amino acids composition (g/100 g proteins) of these subfractions was also  
278 analysed (Table 2). Some subfractions were especially rich in certain amino  
279 acids. This is the case of the high Asp values in F1A, Glu % in F2A and F3B,  
280 high Ser values in F3C and F3D, Arg contents in F1F, Tyr contents in F1F,  
281 Cys contents in F1F, Phe % in F1F and high Lys % in F1C and F1D. With  
282 respect to His contents, highest amounts were observed in subfractions  
283 belonging to fractions F2 and F3. Thus, F2D and F3E with 33.4% and 28.2%  
284 His contents were the subfractions richest in this amino acid. Some of these  
285 subfractions were poor in His, but their binding to the affinity column may be  
286 explained by the presence in high amounts of other amino acids, such as Asp  
287 or Glu, that have also been implicated in the chelating activity of peptides (Lu  
288 et al., 2009)

289

### 290 **3.3. Copper chelating activity**

291 We have studied the copper chelating activity of chickpea purified  
292 peptide fractions. If the degree of binding to the affinity column by chelating  
293 peptides is proportional to their affinity for copper, then it is expected that  
294 fractions more strongly bounded to the column would possess a higher  
295 copper chelating activity. To test this hypothesis, the copper chelating activity of  
296 fractions F1, F2 and F3 was assayed. F3 showed 45.3% chelating activity (Fig.  
297 5A) followed by F2 and F1 with 36.7 % and 28.4 %, respectively. However, F1  
298 had a similar chelating activity than the hydrolysate, that is in accordance with  
299 their similar His contents (Table 2). The chelating activity of these peptide  
300 fractions correlated positively with their elution volume from the affinity column  
301 and with their histidine content (Fig. 5B).

302 Chelating activity of subfractions (F1A-F3D) purified by gel-filtration  
303 chromatography was also analyzed (Fig. 6). In general, sub- fractions of  
304 fractions F2 and F3 showed higher chelating activities. A range of different  
305 chelating activities were observed that are explained not only by the influence of  
306 the His contents, but also by the different peptide sizes. Thus in these  
307 subfraactivity, although this correlation was not as high as in fractions F1, F2 and  
308 F3 (Fig. 7A). On the other hand, no correlation was observed between the  
309 chelating activity and peptide size of these subfractions (Fig. 7B). Fractions with the  
310 highest chelating activity were those that were smaller and with high His contents.  
311 Hence, highest chelating subfractions were F2B (15.3% His and 1205 Da), F3E  
312 (28.3% His and 162 Da), F3D (17.6% His and 308 Da) and F2D (33.4% His and  
313 105 Da). These results suggest that a combination of high His contents, around  
314 20–30%, and small peptide size provide the best chelating activities.

315

#### 316 **4. CONCLUSION**

317 We have shown that chickpea proteins can be hydrolyzed with pepsin  
318 plus pancreatin generating an extensive protein hydrolysate resembling that  
319 produced in humans during food digestion. We have also shown that this  
320 hydrolysate is rich in chelating peptides that can be fast and efficiently purified  
321 by affinity chromatography. Purified chelating peptides are a mixture of peptides  
322 with different amino acid compositions and sizes. We also observed that their  
323 His contents defined more strongly their chelating activity than their size. The  
324 most effective fractions were peptide fractions with His contents above 15%.  
325 The fraction size is not the determinant in the activity although, in general,  
326 smaller fractions showed higher chelating activity. Thus, chelating peptides,  
327 purified from food protein hydrolysates, may be useful in fortifying foods for

328 preventing oxidative activity of prooxidant metals and increasing their  
329 bioavailability while maintaining food quality and appearance.

330

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332

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336

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427 **FIGURE LEGENDS**

428

429 **Figure 1.** Time course of the hydrolysis of chickpea protein isolate with  
430 pepsin (added at time 0 min) and pancreatin (added after 180 min). Data  
431 correspond to the average  $\pm$  SD of three determinations.

432 **Figure 2.** Affinity chromatography purification of chickpea chelating  
433 peptides using a copper charged agarose column.

434 **Figure 3.** Linear correlation between the His content (%) and volume  
435 elution of purified chickpea chelating peptide fractions F1, F2 and F3, from the  
436 copper affinity column.

437 **Figure 4.** Gel filtration chromatography fractionation of chickpea  
438 chelating peptide fractions F1, F2 and F3 purified from the copper affinity  
439 column.

440 **Figure 5. (A)** Copper chelating activity of chickpea protein hydrolysate  
441 and peptide chelating fractions F1, F2 and F3. Data correspond to the average  
442  $\pm$  SD of two independent experiments. **(B)** Linear correlation between copper  
443 chelating activity and His content of protein hydrolysate and chelating peptide  
444 fractions.

445 **Figure 6.** Copper chelating activity of chelating peptide fractions purified  
446 by gel filtration chromatography. Data correspond to the average  $\pm$  SD of two  
447 independent experiments.

448 **Figure 7.** Correlation of copper chelating activity of chelating peptide  
449 subfractions purified by gel filtration chromatography with their His content **(A)**  
450 and their peptide size **(B)**.

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456 **Table 1.** Chemical composition of defatted chickpea flour and protein  
457 isolate. Data expressed as g 100 g<sup>-1</sup> of dry matter are the mean  $\pm$  SD of two  
458 analyses.

459

Components	Defatted flour	Protein isolate
Moisture	5.0 $\pm$ 1.1	tr <sup>a</sup>
Ash	3.5 $\pm$ 0.1	1.3 $\pm$ 0.1
Fibre	25.4 $\pm$ 2.2	5.0 $\pm$ 0.0
Protein content <sup>b</sup>	20.0 $\pm$ 0.3	93.8 $\pm$ 3.3
Lipids	5.8 $\pm$ 0.1	tr
Soluble sugars	1.2 $\pm$ 0.0	tr
Carbohydrates by difference	39.1 $\pm$ 0.0	tr

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461 <sup>a</sup> Trazes

462 <sup>b</sup> Total nitrogen x 6.25

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466

467 **Table 2.** Percent amino acid composition of chickpea protein hydrolysate (PH) and peptide chelating fractions purified by affinity (F1-F3) and gel  
468 filtration chromatography (F1A-F3E).

aa	Asp <sup>a</sup>	Glu <sup>b</sup>	Ser	His	Gly	Thr	Arg	Ala	Pro	Tyr	Val	Met	Cys	Ile	Leu	Phe	Lys
PH	14.1±0.2	18.7±0.0	6.0±0.0	3.0±0.0	4.4±0.0	3.4±0.0	0.5±0.1	4.2±0.1	2.2±0.1	1.5±0.1	4.5±0.1	0.4±0.1	0.5±0.0	4.1±0.1	7.9±0.1	6.65±0.1	6.4±0.1
F1	12.8±0.1	17.3±0.1	3.4±0.0	3.2± 0.0	3.0±0.0	2.4±0.0	24.9±0.3	2.0±0.0	1.3±0.1	1.2± 0.0	1.6± 0.0	0.5±0.1	2.4±0.1	1.8±0.1	3.4±0.0	6.9±0.0	11.7±0.1
F2	14.1±0.6	19.1±0.2	6.2±0.1	17.4±0.1	4.4±0.0	3.1±0.1	5.8±0.2	4.0±0.0	1.3±0.0	0.9±0.0	3.7±0.1	0.2±0.0	1.2±0.0	2.0±0.0	6.9±0.0	4.7±0.1	5.0±0.1
F3	15.6±0.0	16.9±0.1	11.5±0.0	22.9±0.0	3.2±0.0	1.8±0.0	5.9±0.1	2.7±0.0	2.0±0.0	0.3±0.0	1.7±0.0	0.8±0.1	1.1±0.0	4.1±0.2	3.6±0.0	2.3±0.0	3.6±0.0
F1A	24.6±0.8	19.7±4.4	9.1±3.0	3.0±0.3	8.3±2.9	5.9±1.1	4.7±0.9	4.4±1.2	n.d	0.9±0.4	1.4±0.6	0.2±0.3	1.8±0.6	2.9±0.3	6.3±0.1	1.5±0.4	5.3±1.1
F1B	15.9±5.9	31.8±1.4	5.3±0.3	6.2±1.0	4.8±0.2	4.0±0.6	7.1±1.1	2.9±0.5	n.d	0.5±0.0	2.8±0.6	0.5±0.5	1.3±0.1	3.0±0.5	5.7±0.7	2.2± 0.6	6.1± 0.7
F1C	15.9±0.8	16.8±0.2	6.2±0.7	8.1± 0.1	6.3±1.3	3.1±0.4	10.5±1.5	3.9±0.4	n.d	1.2±0.7	2.5± 0.8	0.2±0.1	0.6±0.1	3.2±0.5	5.2±0.3	2.7± 0.5	13.7±0.3
F1D	10.8±1.7	11.8±0.9	5.1±0.7	8.1±0.2	4.8±0.5	2.8±0.8	18.2±3.4	4.1±2.1	n.d	1.9±1.2	1.6±0.2	1.3±1.6	0.8±0.0	2.0±0.7	4.5±0.4	3.5±1.3	18.4±8.7
F1E	9.3± 0.2	11.9±2.3	4.5±1.2	6.3±2.2	4.7±1.4	2.1±0.2	30.9±0.2	3.2±0.8	n.d	1.7±1.7	0.6±0.8	1.2±1.3	2.4±2.5	1.3±0.0	6.2±2.9	5.9±4.3	7.7± 1.1
F1F	6.0± 4.7	5.2±4.6	2.8±3.8	3.6±3.5	4.0±2.9	1.1±1.2	27.5±8.1	1.5±1.3	n.d	12.9±1.3	1.2±0.5	0.6±0.0	6.0±4.8	0.2±0.0	2.4±2.8	21.8±1.9	3.0±2.7
F2A	19.6±0.2	31.3±0.5	8.0± 0.8	8.8± 0.1	4.5±0.3	2.7±0.1	6.4±0.8	2.8±0.2	n.d	0.3± 0.0	0.9±0.9	0.1±0.0	0.2±0.1	2.4±0.3	5.7±0.0	2.2±0.1	3.8± 0.1
F2B	17.1±1.6	23.0±2.0	7.0±1.1	15.3±0.4	4.9±0.2	3.7±0.1	3.9±0.1	4.4±0.1	n.d	1.3± 0.1	1.7±1.5	0.9±0.1	0.5±0.2	2.9±0.1	7.4±0.0	2.7±0.1	3.8±0.5
F2C	14.9±0.8	15.0±2.6	6.4±0.2	23.7±0.7	5.2±0.2	2.0±0.3	5.2±0.9	3.9±0.2	n.d	2.0 ±0.4	2.5±1.7	0.3±0.0	0.5±0.2	1.8±0.2	6.2±0.3	4.9±0.7	5.5±0.4
F2D	10.5±1.8	12.1±0.9	6.6±0.3	33.4±2.3	3.9±0.3	0.9±0.3	7.1±0.9	2.8±0.1	n.d	1.5±0.0	3.4± 2.1	0.2±0.1	0.9±0.5	0.9±0.1	4.7±0.7	8.1±0.9	2.8±0.4
F3A	17.5±0.1	24.4±0.1	7.6±0.3	2.8±0.0	120.±0.1	2.0±0.1	6.3±0.1	3.7±0.0	n.d	0.0±0.0	1.4±0.3	1.0±0.1	0.0±0.0	2.4±0.3	9.9±0.2	2.8±0.0	6.0±0.1
F3B	21.3±0.4	29.6±0.5	9.3±0.3	6.3±0.2	6.8±0.1	2.0±0.0	5.7±0.1	1.1±1.5	n.d	0.0±0.0	0.5±0.0	0.8±0.0	1.6±0.0	1.8±0.0	6.8±0.0	1.1±0.0	5.1±0.1
F3C	20.4±0.7	23.7±0.5	15.0±0.1	8.5±0.1	4.4±0.1	3.0±0.1	5.1±0.1	1.4±2.0	n.d	1.2±0.1	1.7±0.1	0.1±0.1	0.1±0.2	6.3±0.2	4.1±0.1	1.8±0.0	3.0±0.1
F3D	15.3±0.0	15.0±0.1	11.4±0.2	17.6±0.1	5.6±0.0	2.5±0.1	5.2±0.0	4.7±0.1	n.d	0.1±0.0	2.3±0.1	0.0±0.0	0.0±0.0	3.9±0.0	5.7±0.1	4.1±0.0	5.4±0.0
F3E	8.3±0.0	11.0±0.3	8.5±0.1	28.3±0.4	4.6±0.1	2.4±0.0	9.7±0.1	4.0±0.0	n.d	1.4±0.0	2.3±0.1	0.1±0.0	0.1±0.1	1.5±0.0	7.4±0.1	5.2±0.0	4.8±0.2

469 Data correspond to the average ± SD of two independent experiments.

470 <sup>a</sup> Aspartic acid + asparagine.

471 <sup>b</sup> Glutamic acid + glutamine.

472 n.d. Not determined.

473

474 **Table 3.** Peptide size of gel filtration chromatography chelating peptide  
475 fractions. Number of amino acids residues has been calculated on an average  
476 molecular weight of 110 Da per amino acid.

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Gel filtration peptide fractions	Molecular weight (Da)	Number of amino acid residues
F1A	12071	110
F1B	4436	40
F1C	478	4
F1D	296	3
F1E	102	1
F1F	62	1
F2A	2932	27
F2B	1205	11
F2C	281	2-3
F2D	105	1
F3A	5481	50
F3B	768	7
F3C	494	5
F3D	308	3
F3E	162	1-2

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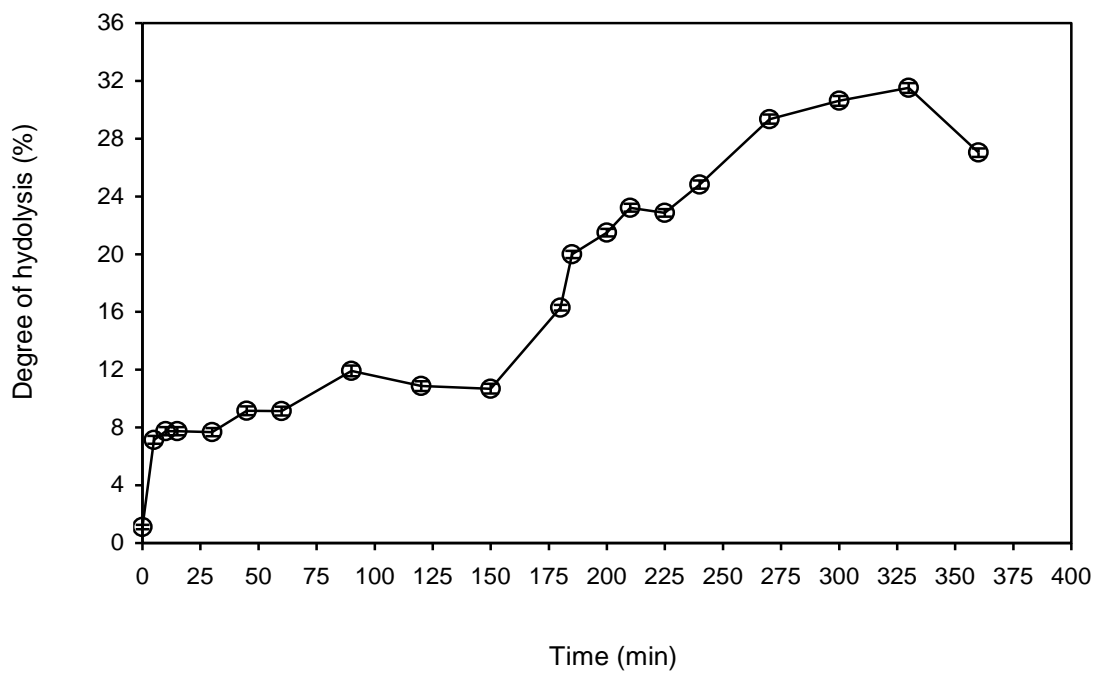
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**Figure 1**

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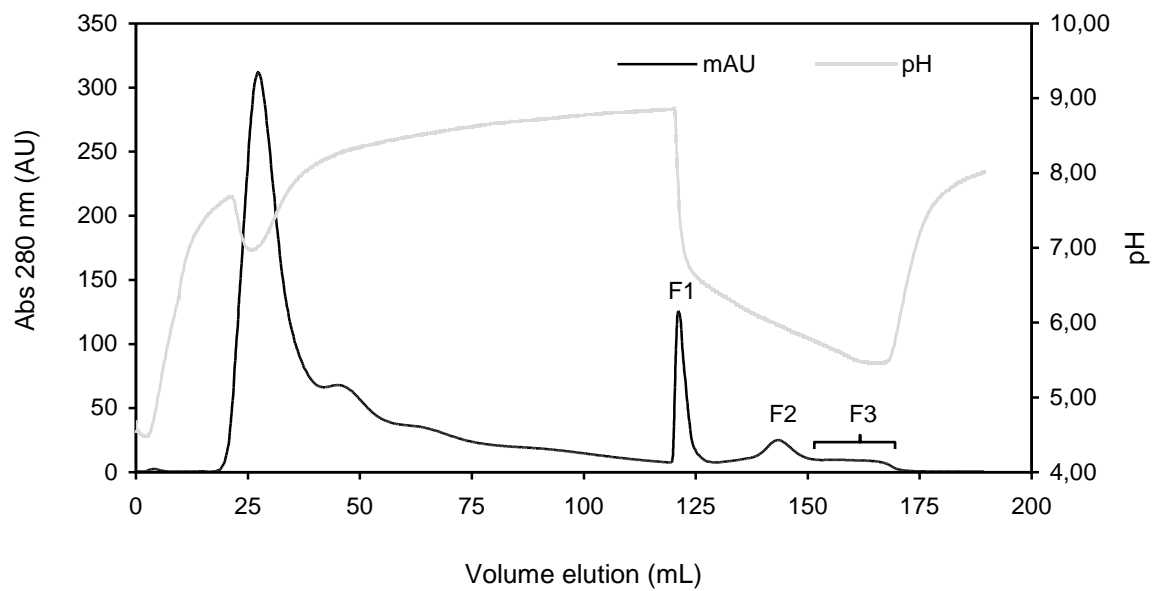
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**Figure 2**

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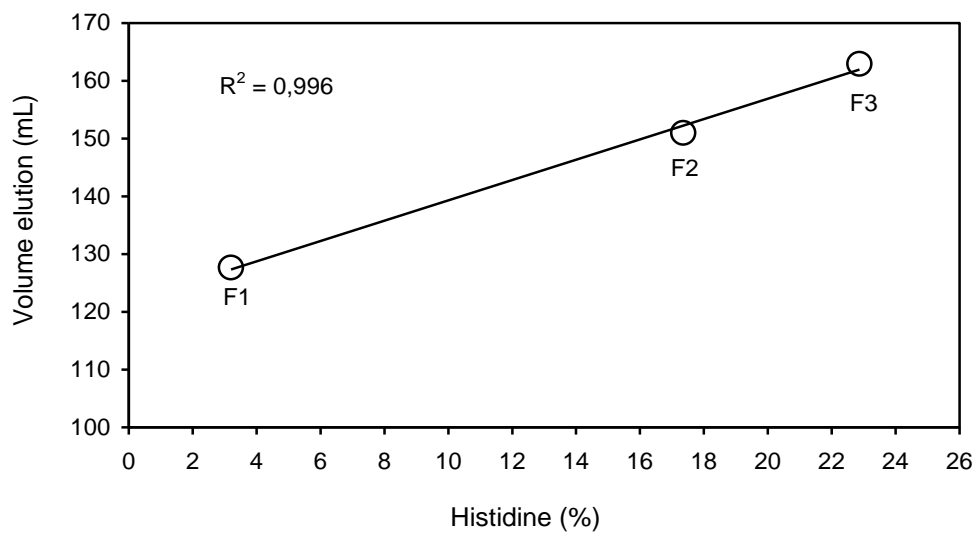
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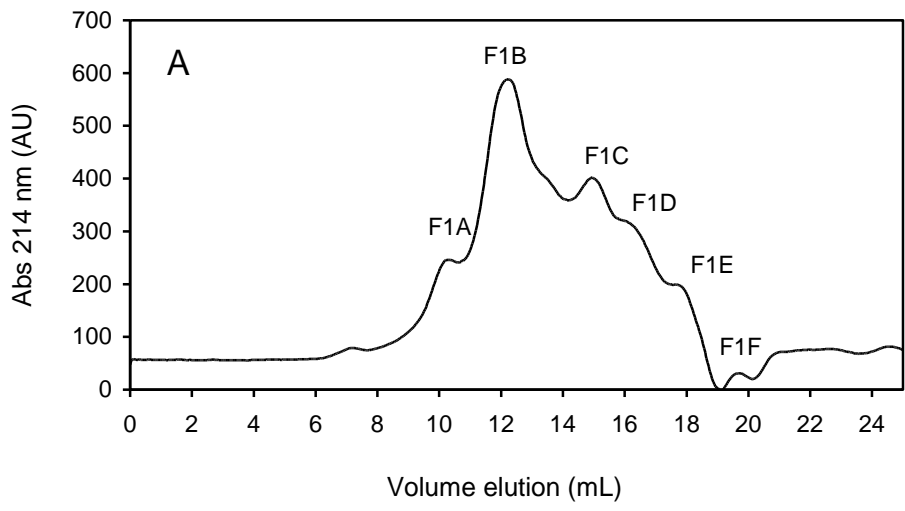
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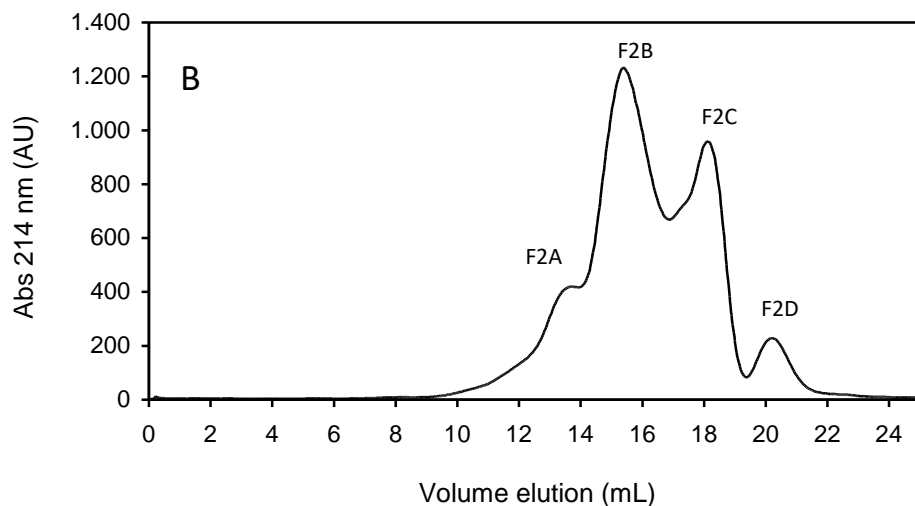
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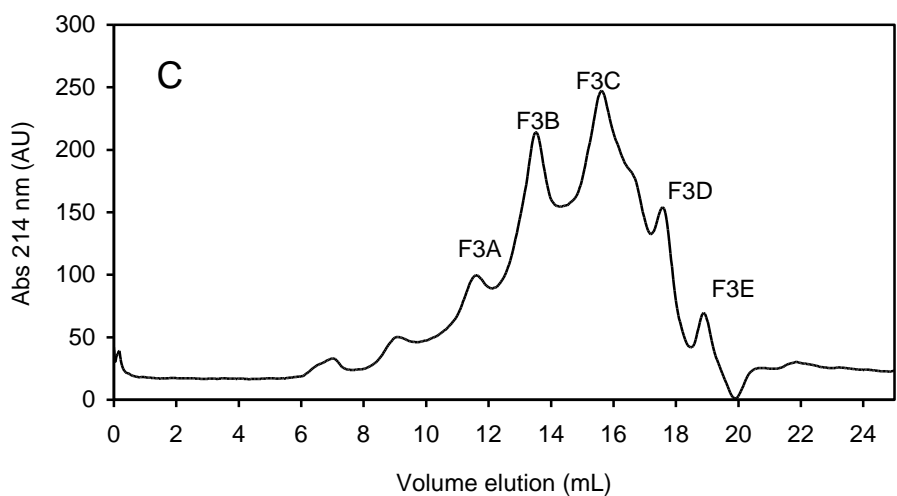
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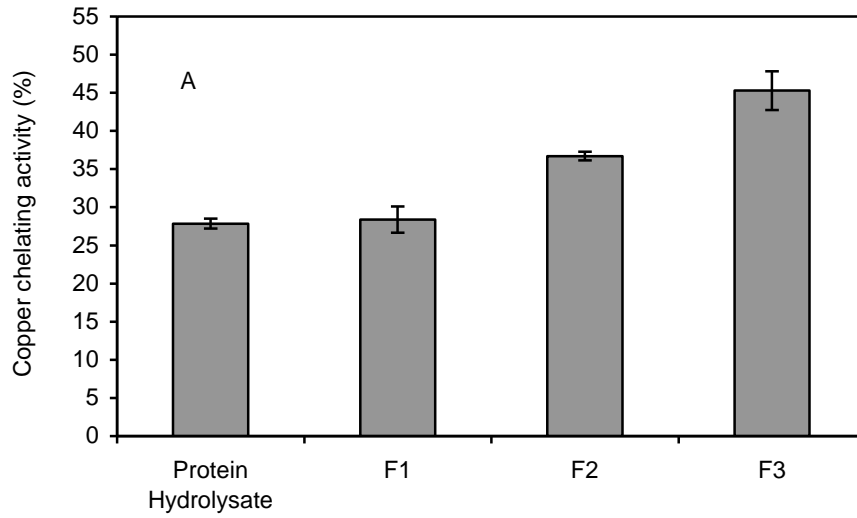
**Figure 4**

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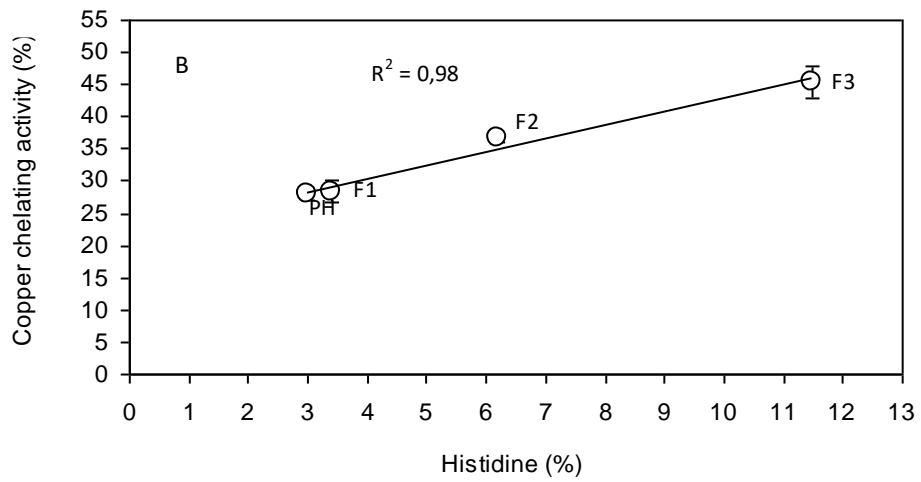
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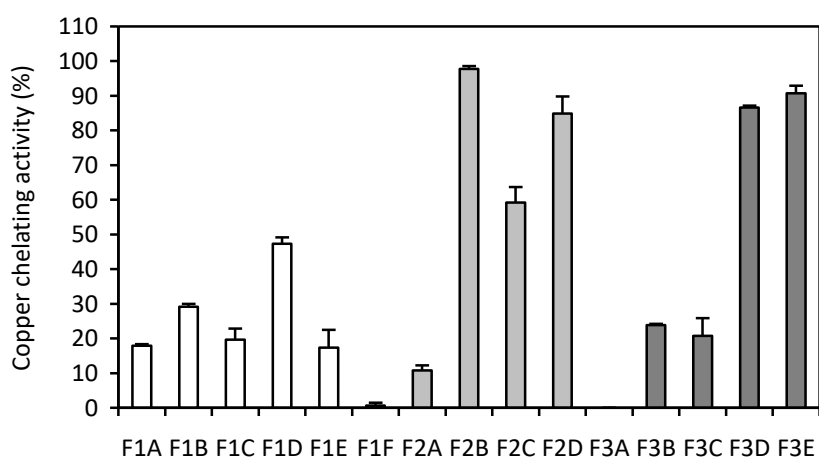
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Figure 5

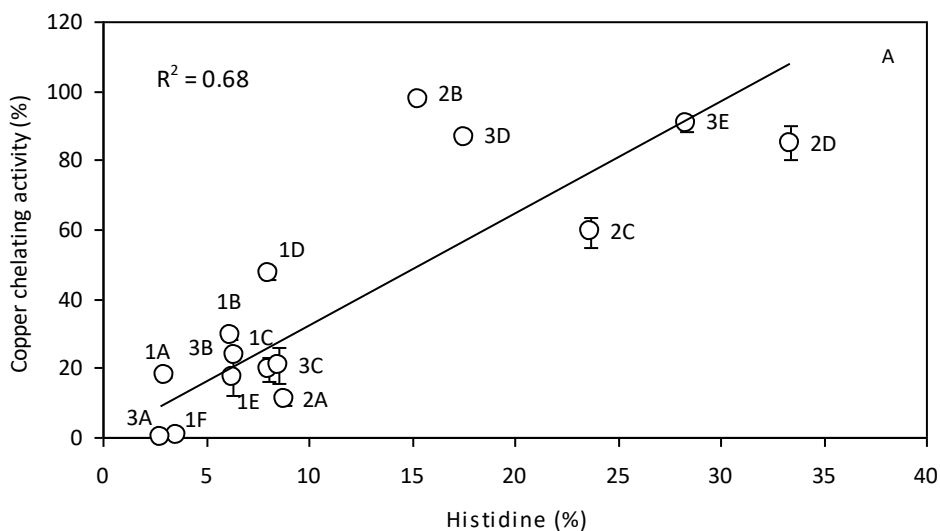
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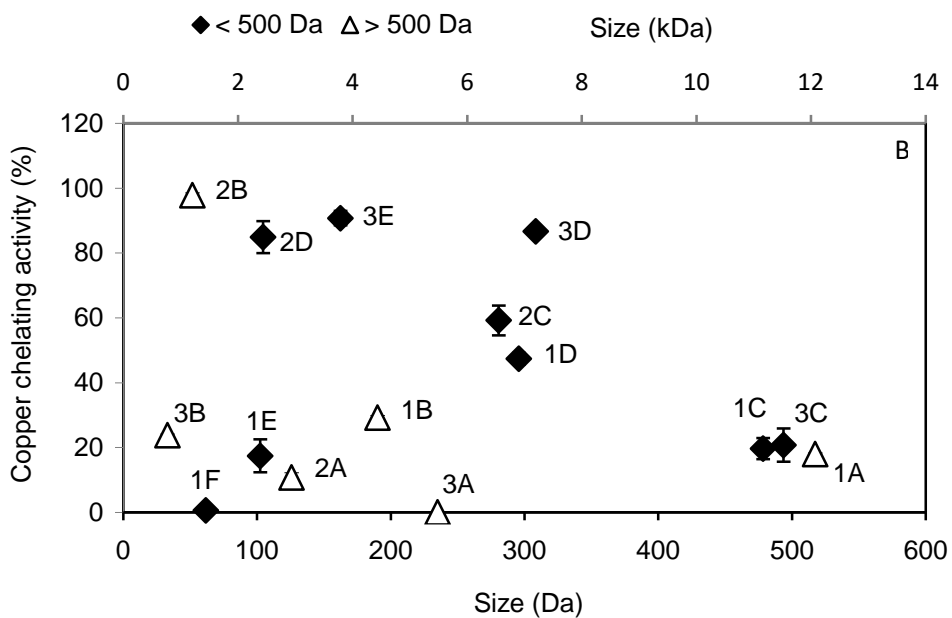
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Figure 6

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Figure 7

